



**COASTAL  
RELIABILITY**  
SOLUTIONS

**PLANNING JOURNAL**

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## VALUABLE PUMP FORMULAS

PRESSURE	PIPE VELOCITY	CENTRIFUGAL PUMPS
Feet of Water X 0.4333 =PSI	Velocity in Feet per Second:	Liquid HP: $\frac{\text{GPM} \times \text{ft. of Head} \times \text{Sp. Gr.}}{3960}$
(PSIX 2.31)/Sp. Gr. =Feet of Water	Rule of Thumb:	Brake HP: $\frac{\text{GPM} \times \text{TDH} \times \text{Sp. Gr.}}{3960 \times \text{Pump Efficiency}}$
(Ft. Head x Sp. Gr.)/2.31 =PSI	Typically, keep pipe velocities around 10 ft/second for good results.	Efficiency $\frac{\text{BHP}}{\text{Overall HP}}$
PSI x 6.9 =kPa	Suction Piping: Generally, have piping in one plane from source tank and have a straight run at least 10 times the pipes diameter leading into the pump suction.	Overall HP: $\frac{\text{BHP}}{\text{Motor Efficiency}}$
ATM x 14.7 =PSI	Pipe Size: Doubling the diameter of a pipe increases its capacity 4 times.	Estimated effects of viscosity on Centrifugal Pumps
ATM x 33.9 =Feet of Water		SSU FLOW HEAD EFFICIENCY
ATM x 760 =mm Hg		35 100% 100% 80%
kg/cm2 x 1.42 =PSI		500 95% 98% 80%
Meters of Water x 1.42 =PSI		1000 92% 97% 70%
Bar x 14.5 =PSI		
Inches of Hg x 0.491 =PSI		

ROTARY POSITIVE DISPLACEMENT PUMPS	APPROXIMATE RPM @ FULL LOAD - FOR MEDIUM SIZED MOTORS
Liquid HP: $\frac{\text{GPM} \times \text{PSI}}{1714}$	Poles RPM (60 Hz) Sync Speed RPM (50 Hz) Sync Speed
Volumetric Efficiency: $\frac{\text{Actual GPM}}{\text{Theoretical GPM}}$	2 3500 3600 2850 3000
Overall Pump Efficiency: $\frac{\text{LHP}}{\text{BHP}}$	4 1750 1800 1450 1500
Mechanical: $\frac{\text{Overall Pump Efficiency}}{\text{Volumetric Efficiency}}$	6 1150 1200 950 1000
	8 850 900 700 750
	Synchronous Speed (no load) Formula RPM = $\frac{\text{Frequency(Hz)} \times 120}{\text{Number of Poles}}$

INSULATION CLASS NEMA 1,15 SERVICE FACTOR	RULES OF THUMB FOR MOTORS
A 150 °C 221 ° F	A motor develops 1.5 ft-lbs per HP @ 3600 RPM A 3-phase motor draws 1.00 Amp per HP @ 557 Volts
B 130 °C 266 ° F	A motor develops 3.0 ft-lbs per HP @ 1800 RPM A 3-phase motor draws 1.25 Amp per HP @ 460 Volts
F 155 °C 311 ° F	A motor develops 4.5 ft-lbs per HP @ 1200 RPM A 3-phase motor draws 2.50 Amp per HP @ 230 Volts
H 180 °C 356 ° F	HP = $\frac{\text{Torque (ft-lbs)} \times \text{RPM}}{5252}$ Torque (in lbs) = $\frac{\text{HP} \times 63,000}{\text{RPM}}$
Maximum motor temperature including temperature rise plus 40° C ambient temperature	

PARTICLE SIZE COMPARISON	ATMOSPHERIC PRESSURE	VISCOSITY	AFFINITY LAWS FOR CENTRIFUGAL PUMPS
Mesh Inch Micron	Altitude in Feet Pressure in PSIA	CONVERSIONS:	These formulas can be used to estimate capacity, head and BHP for a pump speed or impeller diameter when a curve is not readily available:
3250 .0002 6	0 14.70	SSU* = Centistokes x 4.55	1. Flow is directly proportional to the ratio of impeller speed:
1600 .0005 14	100 14.64	Degrees Engler* = Centistokes x 0.132	$\text{GPM}_2 = \text{GPM}_1 \times \frac{\text{RPM}_2}{\text{RPM}_1}$
750 .0010 25	300 14.54	Sec. Redwood 1* = Centistokes x 4.05	2. Head is directly Proportional to the square of the ratio of impeller speed:
325 .0016 40	500 14.43	1 Stoke = 100 Centistokes	$\text{Head}_2 = \text{Head}_1 \times \left( \frac{\text{RPM}_2}{\text{RPM}_1} \right)^2$
250 .0024 62	700 14.33	1 Poise = 100 Centipoises	3. The HP is directly proportional to the ratio of impeller speed:
200 .0029 74	1,000 14.17	Centistokes = Centipoise/Sp. Gr	$\text{BHP}_2 = \text{BHP}_1 \times \left( \frac{\text{RPM}_2}{\text{RPM}_1} \right)^3$
180 .0033 85	1,500 13.92	*Where Centistokes are greater than 50	4. Flow is directly proportional to the ratio of impeller diameter:
150 .0041 100	2,000 13.66	Definitions:	$\text{Flow}_2 = \text{Flow}_1 \times \left( \frac{\text{Impeller Diameter}_2}{\text{Impeller Diameter}_1} \right)^3$
120 .0046 118	3,000 13.17	Newtonian fluids are unaffected by shear, e.g. water, mineral oil.	5. Head is directly proportional to the square of the ratio of Impeller diameter:
100 .0055 149	4,000 12.69	Non-Newtonian fluids are affected by shear (5 types).	$\text{Head}_2 = \text{Head}_1 \times \left( \frac{\text{Impeller Diameter}_2}{\text{Impeller Diameter}_1} \right)^2$
80 .0070 179	5,000 12.23	Bingham-Plastic fluids have an exact shear point which once exceeded, viscosity decreases.	6. The HP is directly proportional to the cube of the ratio of impeller diameter:
50 .0117 300	7,000 11.34	Pseudo-Plastic fluids have no exact yield point, but instead, viscosity decreases as the magnitude of shear rate increases.	$\text{BHP}_2 = \text{BHP}_1 \times \left( \frac{\text{Impeller Diameter}_2}{\text{Impeller Diameter}_1} \right)^3$
40 .0150 385	10,000 10.11	Dilatant fluids viscosity increases as the magnitude of the shear rate increases, e.g. printing ink, candy compounds.	
30 .0200 513	15,000 8.29	Thixotropic fluids decrease in viscosity both in relation to the shear magnitude and the period of time subjected to shear. Viscosity might also depend on a previous shear condition, e.g. drilling mud, starches, paint.	
24 .0280 718	20,000 6.76	Rheopectic fluids increase viscosity both in relation to the shear magnitude and the period of time subjected to shear, e.g. some greases,	
20 .0340 872	25,000 5.45		
18 .0390 1000	30,000 4.36		
16 .0450 1154	40,000 2.72		
14 .0510 1308	50,000 1.68		
12 .0600 1538	60,000 1.04		
10 .0750 1923			
8 .0970 2488			
6 .1320 3385			
4 .1590 4077			
2 .2630 5205			
1 Micron = 10 <sup>-6</sup> Meters			
1 Micron = 3.9 x 10 <sup>-4</sup> inch			



## PROUDLY REPRESENTING

INDUSTRIAL & MUNICIPAL PUMPS • MECHANICAL SEALS • MECHANICAL PACKING  
NON-METALLIC TANKS • HEAT EXCHANGERS • COMPRESSORS



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PUMPS	Abaque	Industrial Hose Pumps (Peristaltic)
	Ansimag	ANSI Non-Metallic Pumps, Sub-ANSI Non-Metallic, Self-Priming Non-Metallic Pumps and Non-Metallic Mag-Drive Pumps
	Aplex Myers	Medium and Heavy Duty Reciprocating Pumps (up to 5500 PSI and up to 600 GPM)
	Aurora	ANSI Centrifugal Pumps, Regenerative Turbine Pumps, End Suction Pumps, Inline Pumps, Multi-Stage Vertical Pumps, Split Case Pumps, Boiler Feed Pumps, Sump Pumps, Sewer Pumps, Booster Systems and Condensate Systems
	Blackmer	Positive Displacement Sliding Vane Pumps, Mouvex CIP Pumps, System One Pumps, Mag-Drive Pumps, Abaque Peristaltic Hose Pumps, Horizontal and Vertical Pumps and Vortex Pumps
	Fairbanks Nijhuis	Internal Gear Pumps, Mag-Drive Gear Pumps, Chemical Gear Pumps, Asphalt Gear Pumps
		Turbine Pumps, Split Case Pumps, Vertical Inline Pumps, Propeller Pumps, Solids-Handling Pumps, Submersible Pumps and Fire Pumps
	Grindex	Dewatering Pumps and Electric Submersible Pumps (up to 370' and up to 5200 GPM)
	HMD Kontro	Metallic Mag-Drive Pumps and High Pressure Mag-Drive Pumps
	Jesco Pump (Lutz)	Industrial and Municipal Metering Pumps, Drum Pumps, AOD Pumps and Non-Metallic Pumps
	Landustrie	Submersible Pumps, Centrifugal Pumps, Vortex Pumps, Screw Pumps and Submersible Mixers
	Layne Mid-America	Vertical Pumps and Turbine Pumps
	Megator / P2K	Sliding Shoe Pumps, Rotary Lobe Pumps, Floating Strainers, Oil Recovery Units & Skimmers, Pneumatic Diaphragm Pumps and Double Diaphragm Pumps
	Myers	Submersible Pumps, Centrifugal Pumps, Vortex Pumps and Self-Priming Pumps
	Nikkiso / LEWA	Non-Seal® Pumps, Canned Motor Pumps, API-685 Hydraulically Actuated Diaphragm Pumps
	Pitbull Pumps	Air-Operated Positive Displacement Pumps
	Summit Pump	ANSI Pumps, Regenerative Turbine Pumps, Self-Priming Pumps, Trash Pumps, Slurry Pumps, Progressive Cavity Pumps, Split Case Pumps and Aftermarket Parts
	Sundyne / Marelli	Heavy Duty Split Case API 610 Pumps, Multi-Stage Pumps, End-suction Horizontal Single and Double Volute Pumps, Axially Split Pumps and Submersible Pumps
	Sundyne / Sunflo	High Speed/High Pressure Pumps, API Pumps, High Speed Compressors, Blowers and Custom Integrated Skid Systems
	Versa-Matic	AODD Pumps (Bolted, Clamped, Non-Metallic, Metallic and Sanitary 3A)
	Vertiflo Pumps	Vertical Vortex Pumps, Cantilever Pumps, High Chrome Iron Pumps. Centrifugal Pumps and Self-Priming Pumps
MECHANICAL SEALS, PACKING & SEALING DEVICES	Flex-A-Seal	Mechanical Seals, Packing, Gaskets and OEM Quality Repairs of All Types and Manufactures
		Triple Lip Mechanical Seals and Dry Run Mechanical Seals
	Palmetto	Pump and Valve Packing (Graphite, GFO Fiber, PTFE, Carbon, Phenolic and more), Custom Cut and Sheet Gasketing and Non-Asbestos Gasketing
	Seal Pots	Barrier Fluid Pots (ANSI/API, Heat Exchangers, Forced Circulation Loop Systems)
HEAT EXCHANGERS	Hexonic	Shell & Coil, Shell & Tube, Brazed Plate, SafePlate Double Wall, Plate & Frame,CIP/3A Sanitary, TEMA, Custom and Bio-Mass Heat Exchangers
COMPRESSORS	Blackmer	Reciprocating Compressors, Oil-Free Compressors and Single and Double Cylinder Compressors
	PPI	Sealless Diaphragm Compressors
	Sundyne	Centrifugal Compressors, Integrally Geared Compressors, Multi-Stage Compressors and Vertical Line Mounted Compressors
TANKS	Allen Industries	Fiberglass Reinforced Plastic Tanks and Repair Service
	Assmann	Polyethylene Tanks, Linear and Crosslink, Single Wall Tanks, Double Wall Tanks, Conical Bottom Tanks, Vertical and Horizontal Tanks, Full Drain (FDO) Tanks, Chemical Feed Systems and Secondary Containment Tanks (ISO Certified, NSF Approved for Water and Chemical Storage)
EXPANSION JOINTS	FlexHose	Metal Bellows Expansion Joints and Custom Designed Expansion Joints
DAMPENERS	LUTZ Jesco Versamatic	Pulsation Dampeners, Suction Stabilizers, Surge Absorbers and Expansion Compensators
VALVES	Maric Valves	Precision Flow Control Valves and Constant Flow Valves (Regardless of Pressure)
	Valves	Ball Valves, Butterfly Valves, Flapper Valves, Gate Valves, 3-Way Valves, Pinch Valves, Knife Valves, Sanitary Valves, Back Pressure and Pressure Relief Valve



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JAN FEB MAR APR MAY JUN 1 2 3 4 5 6 7 8 9 10 11 12 13 14 15 16  
JUL AUG SEP OCT NOV DEC 17 18 19 20 21 22 23 24 25 26 27 28 29 30 31

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